The listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

- 1. (Cancelled)
- 2. (Previously Presented) A process according to claim 14, comprising 4 reactors arranged in series.
- 3. (Previously Presented) A process according to claim 2, wherein each of the reactors of the series is supplied directly by the regenerated catalyst obtained from the regeneration zone.
- 4. (Previously Presented) A process according to claim 2, wherein the regenerated catalyst from said common distribution zone directly supplies only the first and the third reactors of the series, whereby the numbering is done in the order that the feedstock and intermediate effluents pass through, whereby the second reactor of the series is supplied by the catalyst obtained from the first reactor of the series, and whereby the fourth reactor is supplied by the catalyst obtained from the third reactor of the series.
- 5. (Previously Presented) A process according to claim 2, wherein the regenerated catalyst directly supplies only the first and the fourth reactors of the series, whereby the numbering is done in the order that the feedstock and intermediate effluents pass through, whereby the second reactor of the series is supplied by the catalyst obtained from the first reactor of the series, and whereby the third reactor of the series is supplied by the catalyst obtained from the second reactor of the series.
- 6. (Previously Presented) A process according to claim 2, wherein the regenerated catalyst supplies each of the four reactors, and the spent catalyst is collected from only a group of two reactors.

- 7. (Previously Presented) A process according to claim 14, wherein the operating pressure is less than 0.2 MPa absolute.
- 8. (Previously Presented) A process according to claim 14, wherein the H2/HC molar ratio is less than 2.
- 9. (Previously Presented) A process according to claim 14, wherein the volumetric flow rate is greater than 2 h⁻¹.
- 10. (Currently Amended) A process according to claim 14, In a regenerative reforming process for treatment of hydrocarbon fractions comprising a series of at least two reactors forming a reaction zone, wherein feedstock and intermediate effluents pass through the reactors in succession and each reactor operates as a moving bed, the process having a regeneration zone for eliminating coke deposited on the catalyst during reactions, the improvement comprising passing coked catalysts of the same chemical type but having different amounts of coke from the outlet of said at least two reactors to a common mixing zone and homogenizing said coked catalysts so as to provide a mean coke concentration, and passing the resultant homogenized catalysts to said regeneration zone, and passing the resultant regenerated catalysts obtained from said regeneration zone directly to a common distribution zone and distributing the regenerated catalysts from said common distribution zone to said at least two reactors, and further comprising a source of air for operating instruments and employing a portion of the instrument air, for the combustion of the coke deposited on the catalyst in the regeneration zone.
- 11. (Previously Presented) A process according to claim 14, wherein the reactors that form the series of reactors are placed side by side.
- 12. (Previously Presented) A process according to claim 14, wherein the reactors that form the series of reactors are stacked vertically on one another.

- 13. (Previously Presented) A process according to claim 14, comprising aromatization or dehydrogenation of normal paraffins.
- 14. (Previously Presented) In a regenerative reforming process for treatment of hydrocarbon fractions comprising a series of at least two reactors forming a reaction zone, wherein feedstock and intermediate effluents pass through the reactors in succession and each reactor operates as a moving bed, the process having a regeneration zone for eliminating coke deposited on the catalyst during reactions, the improvement comprising passing coked catalysts of the same chemical type but having different amounts of coke from the outlet of said at least two reactors to a common mixing zone and homogenizing said coked catalysts so as to provide a mean coke concentration, and passing the resultant homogenized catalysts to said regeneration zone, and passing the resultant regenerated catalysts obtained from said regeneration zone directly to a common distribution zone and distributing the regenerated catalysts from said common distribution zone to said at least two reactors.
- 15. (Previously Presented) A process according to claim 14, wherein said homogenizing of the coke containing catalysts is conducted by passing said catalysts to a fluidized zone.
- 16. (Previously Presented) A process according to claim 14, wherein said homogenizing of the coke containing catalysts is conducted by passing said catalyst to multimixing zone.
- 17. (Previously Presented) A process according to claim 14, wherein the regenerated catalyst is subjected to reduction in the common distribution zone.
- 18. (Previously Presented) A process according to claim 14, wherein the catalyst in the distribution zone is homogeneous.

- 19. (Previously Presented) A process according to claim 14, wherein the catalyst in the distribution zone is not subjected to a separation step so as to provide different types of catalysts.
- 20. (Previously Presented) A process according to claim 14, wherein the catalyst is passed from the distribution zone directly to said at least two reactors, optionally reduced in an intermediate reduction step.
- 21. (Previously Presented) A process according to claim 17 further comprising subjecting the catalyst to a further reduction step prior to being introduced into the reactors.